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### (54) Emission control system for an internal combustion engine

Abgasreinigungseinrichtung einer Brennkraftmaschine

Dispositif de réglage des émissions pour moteurs à combustion interne

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## Description

**[0001]** This invention concerns improvements in emission control, especially for vehicles or stationary engines, which may be powered by gasoline, diesel, natural gas or other hydrocarbon or oxygenate fuels. The invention will be described hereinafter with particular reference to gasoline-fuelled engines, but is not to be considered to be limited thereto.

**[0002]** As emissions from gasoline engines become more regulated, attention has been concentrated on the start-up phase, when emissions of hydrocarbons ("HCs") tend to be highest, because the catalyst has not reached a temperature giving a reasonable conversion efficiency ("light-off"). The "light-off" temperature is considered to be the temperature at which 50% of the emissions are converted. A variety of methods have been proposed to improve cold start emission control, including electrical heating of the catalyst or gas entering the catalyst, and trapping hydrocarbons until the catalyst reaches light-off temperature, whereupon the hydrocarbons are released for oxidation. For example, USP 5,078,979 proposes a combination of catalyst and HC trap, wherein the trap may be a zeolite selected to have a greater absorption capacity for HCs than for water.

**[0003]** It is known that water present on the hydrocarbon trap and/or catalyst component and/or present in the exhaust gas itself can reduce the performance of the component.

**[0004]** For example, US Patent 5,417,947 describes an emission control system in which olefins are particularly targeted, because of their propensity to form ozone in the atmosphere. This patent teaches a system to remove olefins includes a hydrophilic material to remove at least some of the water from the exhaust gas, a hydrocarbon trap downstream thereof, and a catalyst downstream of the hydrocarbon trap.

**[0005]** This arrangement can limit the amount water produced in combustion from reaching the hydrocarbon trap and/or the catalyst so that exhaust gas treatment during cold start is improved.

**[0006]** DE 41 39 600 A describes a exhaust system without a hydrocarbon trap in which in one embodiment ambient air is heated using a fuel burner and the heated air is flowed over a catalyst in the exhaust system prior to or at, start up thereby to heat the catalyst to light-off more rapidly.

**[0007]** An earlier proposal in this general field is found in DE 2129209, in which an exhaust gas from an engine operated at a rich fuel-air ratio to reduce NO<sub>x</sub> formation is cooled, hydrocarbons are adsorbed and then CO is oxidised over a catalyst such as "Hopcalite". The adsorber is regenerated and the hydrocarbons are recycled to the engine carburettor. This concept runs counter to modern engine and emission control design, and is not believed to offer a practical way of meeting current emissions regulations.

**[0008]** We have confirmed that the presence of water adversely affects the ability of suitable HC trap materials to adsorb HCs, with the consequence that the overall performance of the system in dealing with emissions during cold start, or before light-off, is reduced. We have also confirmed that pre-drying the HC trap and the catalyst system itself prior to cold start, leads to substantial improvements in the overall performance of the system. This may be achieved by pre-drying means, such as a pump to provide a stream of air (eg at 350-500°C) after switch-off of the engine, which air may be heated by residual heat from the catalyst or engine.

**[0009]** We have now discovered that if water is removed from air used to dry the hydrocarbon trap and/or catalyst using a water trap, a further improvement in emission control during cold-start can be achieved.

**[0010]** According to one aspect, the present invention provides a device which the features of claim 1.

**[0011]** According to a further aspect, the invention includes a method which the features of claim 11.

**[0012]** Preferably, the performance of the dried HC trap and/or catalyst system is further improved by incorporating water trapping. A water trap positioned upstream of a HC trap and catalyst system can provide a practical engine emission control system with close to substantially theoretical emission control efficiency.

**[0013]** A suitable catalyst is a highly loaded Pd- or Pt-based catalyst although any catalyst material with low light-off characteristics may be used. It may alone, or in combination with one or more other catalyst components, oxidise CO and HCs and reduce NO<sub>x</sub>. The actual catalyst used is not believed to be critical to the present invention.

**[0014]** A suitable HC trap material is an ion-exchanged zeolite, such as Co/ZSM-5 or Pt/ZSM-5, but other HC traps including impregnated zeolites and non-metallised zeolites, may be used. Preferred HC trap materials are those which also are effective to have a trapping or delaying effect on NO, and metallised zeolites are especially suitable. The material known as silicalite, or very high silica/alumina ratio aluminosilicates, are cost-effective HC traps.

**[0015]** A suitable water trap is a water trapping molecular sieve, such as a zeolite 5A, although zeolite 3A, 4A or 13X may be used. Most zeolites preferentially adsorb water in comparison to HCs, but in general the smaller pore size zeolites are preferred. Other high surface area materials, including particularly silicas and aluminas, may exhibit better properties than zeolites after hydrothermal ageing in use. The water trap and the HC trap may be of the same material.

**[0016]** We have found that both NO and hydrocarbon species can severely inhibit the activity of low light-off CO oxidising catalysts. HC and NO are, of course, natural components of exhaust gas. The present invention further provides a HC trap and catalyst combination wherein the catalyst comprises a low light off temperature CO oxidation catalyst and the combination is so arranged that said catalyst is not exposed to sufficient concentration of HC, and preferably, is not exposed to sufficient concentrations of NO, that CO oxidation on said catalyst is substantially inhibited

during light-off. Naturally, the presence of an upstream water trap will also lower the exposure of said catalyst to water; this may also lead to a benefit at light-off. Most preferably, the CO concentration of the exhaust gas is sufficiently high for the oxidation reaction exotherm heat of reaction to raise the catalyst temperature sufficiently high to oxidise hydrocarbons (HCs) as the said HCs desorb from that HC trap. It may be preferable to modify the engine operating regime to provide for higher than normal CO emissions during cold start, in order to maximise the CO oxidation exotherm. This may be achieved by modifying the electronic engine management system, *eg* by revising the memory and/or control circuitry on the engine management "chip", which may be carried out by those skilled in the art.

[0017] A particularly suitable configuration for a preferred embodiment is a water trap followed by a HC trap and a catalyst, optionally within a single "can" or exhaust system box, or there may be a mixed or layered trap and catalyst, for example a portion of the catalyst is coated with a porous material that permits CO and oxygen to reach the catalyst surface, but prevents HC reaching the catalyst surface. A simpler arrangement is where trap material is admixed with the catalyst. Preferably, however, the water trap and HC trap are deposited on separate monolith supports, as described in more detail below.

[0018] The invention further provides an exhaust gas emission control system comprising a water trap, a HC trap, a catalyst which is a low temperature light -off CO oxidation catalyst, a catalyst which is a low temperature light-off HC oxidation catalyst, and means for pre-drying the system, so arranged that the exotherm from CO oxidation is effective to raise the temperature of the HC oxidation catalyst. The CO and HC catalysts may be the same catalyst formulation, or different components may provide the two different duties. For example, the low temperature light-off CO oxidation may be coated with a porous layer, which permits CO and O<sub>2</sub> to reach the catalyst surface, but prevents HC from reaching the surface.

[0019] The effectiveness of the total emission system of the above preferred embodiment during cold start is substantially improved by pre-drying the system before the cold start. This may be achieved by pre-drying means, such as a pump to provide a stream of air after switch-off of the engine. Optimally, the residual engine or exhaust heat, or heat from the catalyst, may be used.

[0020] In a particularly preferred embodiment, the pre-drying means incorporates a secondary water trap to dry the air from the pump for the duty of drying the main water trap. The secondary water trap may be dried or regenerated during engine operation by utilising waste heat, *eg* from the engine, and a relatively low flow of air from the pump. It may be desirable to incorporate a water trap positioned downstream of the catalyst, to prevent moist ambient air travelling back up the exhaust system to reduce the effectiveness of the catalyst and/or HC trap.

[0021] The water trap, HC trap and catalyst, whether as discrete units or with one or more layered components, may be manufactured according to generally known methods in the catalytic converter art. Preferably, each component, whether as a discrete unit or a layered unit, is in the form of a deposit on the surfaces of an open-celled honeycomb support, which may be metal or a ceramic such as corundum. Such supports are commercially available or may be manufactured according to known methods, and demonstrate low resistance to flow of exhaust gases.

[0022] It may be desirable, according to the present invention, to provide pre-drying means such as a stream of electrically heated air for drying the HC trap and/or catalyst in the event of the emission control system having stood for several days, or generally under conditions under which the trap and/or catalyst have been exposed to ambient air and have adsorbed moisture.

[0023] We believe that the present invention will demonstrate more considerable benefits in the case of used or "aged" catalysts than with brand new catalysts.

[0024] Further details of the present invention, and an appreciation of its various aspects may be seen from the accompanying drawings, in which:

Figures 1 to 5 are plots showing conversions of CO and hydrocarbons over a standard commercial low light-off catalyst containing Pd on alumina/ceria/zirconia particles, mixed with a HC trap, and show levels of pollutants remaining in the gas downstream of the catalyst.

Figure 6 is a similar plot, but when operating according to the present invention.

Figures 7 and 8 are plots showing the effect on CO conversion when a HC trap is used, and

Figure 9 is a schematic diagram of an emission control system according to one embodiment of the present invention.

[0025] In order that the invention may be more fully understood, reference is made to the accompanying Examples by way of illustration only. Examples in which air used to dry the HC trap and/or the catalyst is not itself dry are provided for the purposes of comparison only.

## TEST 1

[0026] Referring firstly to Figure 1, a synthetic exhaust gas composed of

400ppm	C <sub>3</sub> H <sub>6</sub>
80ppm	C <sub>7</sub> H <sub>8</sub> (toluene)
500ppm	NO
5000ppm	CO
8000ppm	O <sub>2</sub>
10%	H <sub>2</sub> O
balance argon	

is passed over a powder sample of catalyst A, (10% Pd on alumina/ceria/zirconia), at a space velocity equivalent to 30,000hr<sup>-1</sup> through a catalyst-coated monolith. The gas inlet temperature was increased at a ramp rate of 100°C/minute, from 40°C to 300°C. The product gas was analysed with respect to time, for CO, C<sub>3</sub>H<sub>6</sub> and C<sub>7</sub>H<sub>8</sub> and the results plotted on Figure 1.

## TEST 2

[0027] Referring now to Figure 2, the same arrangement and general test conditions were used with a physical mixture of 2 parts of 2% Co/ZSM-5 prepared by ion-exchange, and 1 part of catalyst A in the reactor. It can be seen that CO conversion is very similar to that of Test 1, but that, especially in the first 25 seconds, quantities of the hydrocarbons C<sub>3</sub>H<sub>6</sub> are very much lower than in Figure 1 due to trapping in the Co/ZSM-5 zeolite. C<sub>3</sub>H<sub>6</sub> is released as temperature is increased, but C<sub>7</sub>H<sub>8</sub> either remains trapped or is catalytically converted until there is a small amount detected after 100 seconds. Clearly, a hydrocarbon trap is effective.

## TEST 3

[0028] The same general test conditions and same catalyst/trap mix as in Test 2 is used, but the catalyst/trap system has been pre-dried by heating to 450°C and flushing with air for 5 minutes, then cooled to 40°C prior to the start of the run. The results are shown in Figure 3.

[0029] It can readily be seen, in comparison to Figures 1 and 2, that there is a dramatic reduction in the pollutant gases, especially during the early part of the test, and the total quantity of C<sub>3</sub>H<sub>6</sub> is reduced.

## TEST 4

[0030] The same general test conditions and catalyst/trap mix as in Tests 2 and 3 are used, but the catalyst/trap mix was pre-dried and there is 0% H<sub>2</sub>O in the gas. Figure 4 demonstrates dramatically that removing H<sub>2</sub>O could essentially eliminate the emissions of the studied pollutants from the catalyst during start-up.

## TEST 5

[0031] The same test conditions as in Test 4 are used, but instead of Co/ZSM-5 being a component of the trap/catalyst, the same quantity of silicalite is used. As in Test 4, the trap/catalyst was pre-dried. The results are plotted in Figure 5, and it can be seen that silicalite is also effective in reducing start-up emissions, although less effective than Co/ZSM-5.

## TEST 6

[0032] Reverting to the initial gas mixture (see Test 1), and using a water trap (zeolite 5A) upstream of the catalyst/HC trap (Co/ZSM-5). The weight ratio of water trap/hydrocarbon trap/catalyst is 4:2:1. The system was pre-dried as with Test 3. All other variables were unchanged from Test 3. The results shown in Figure 6, compared with Figure 3, shows virtually complete reduction in total quantities of the pollutants from a realistic synthetic exhaust gas mix.

## TEST 7

[0033] A reactor was filled with particles of catalyst A and tested for CO conversion for a variety of feed compositions;

CO/O<sub>2</sub> = 5000/6000 (ppm), balance N<sub>2</sub>

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CO/C<sub>3</sub>H<sub>6</sub>/O<sub>2</sub> = 5000/300/6000 (ppm), balance N<sub>2</sub>  
 CO/NO/O<sub>2</sub> = 5000/500/6000 (ppm), balance N<sub>2</sub>  
 CO/NO/C<sub>3</sub>H<sub>6</sub>/O<sub>2</sub> = 5000/500/300/6000 (ppm), balance N<sub>2</sub>.

[0034] The temperature was ramped at 5°C/min, and the space velocity was equivalent to 45,000hr<sup>-1</sup> over a catalyst-coated monolith. The results show that the CO/O<sub>2</sub> feed reaches 50% conversion (considered to be the "light-off" temperature) at approximately 92°C; the CO/NO/O<sub>2</sub> feed reaches light-off at approximately 135°C; the CO/C<sub>3</sub>H<sub>6</sub>/O<sub>2</sub> feed reaches light-off at approximately 139°C, and the CO/NO/C<sub>3</sub>H<sub>6</sub>/O<sub>2</sub> feed does not reach light-off until 171°C.

[0035] We have concluded from these results that CO light-off is inhibited by hydrocarbon (C<sub>3</sub>H<sub>6</sub>) and NO, and that removal of at least hydrocarbon from a gas stream will improve CO light-off. Preferably, of course, the emission control system would be arranged such that both NO and hydrocarbon species did not reach the catalyst during the CO light-off phase. The trapping of NO by a material within the system provides significant benefits during CO light off.

### TEST 8

[0036] A bed of silicalite was incorporated upstream of a fully formulated commercial low light-off catalyst (weight ratio 4:1). The space velocity is equivalent to 25,000hr<sup>-1</sup> and the temperature ramp is approximately 40°C/min. The feed gas is 7000ppm CO, 150ppm C<sub>3</sub>H<sub>6</sub>, 10,000ppm O<sub>2</sub>, balance He. CO conversion was measured against temperature, and plotted in Figure 8; for comparison, the identical test was performed without using silicalite, and it can be seen that removing hydrocarbons by a silicalite trap improves CO light-off and total CO conversion.

### TEST 9

[0037] The reactor is packed with a zeolite 5A water trap, upstream of a silicalite/catalyst A mix in a weight ratio of 4:2:1 (zeolite:silicalite:catalyst), which is compared with a sample of catalyst A alone.

[0038] Samples of gas are passed through the reactor at a space velocity which is equivalent to a space velocity of 60,000hr<sup>-1</sup> through a catalyst-coated monolith. The system is pre-dried at 450°C as described above. The reactor is heated at a ramp rate of 100°C/min from 40°C to 300°C, whilst a gas mixture which is either "high" in CO content, or "low" in CO content is passed through for 150 seconds. The O<sub>2</sub> content of the gas was also adjusted to keep the overall air/fuel ratio approximately constant.

[0039] Gas compositions are shown in Table 1 below, and the total emission of CO and C<sub>3</sub>H<sub>6</sub> for the first 150 seconds are shown in Table 2 below.

TABLE 1:

Gas Compositions	
Lower CO Concentration	Higher CO Concentration
400ppm C <sub>3</sub> H <sub>6</sub>	400ppm C <sub>3</sub> H <sub>6</sub>
500ppm NO	500ppm NO
5000ppm CO	18400ppm CO
8000ppm O <sub>2</sub>	16700ppm O <sub>2</sub>
10% H <sub>2</sub> O	10% H <sub>2</sub> O
balance Argon	balance Argon.

TABLE 2:

CO and C <sub>3</sub> H <sub>6</sub> emissions during test cycle (first 150 seconds)		
	CO (mg)	C <sub>3</sub> H <sub>6</sub> (mg)
Blank (no catalyst) low CO feed	8.7	1.04
Catalyst only, low CO feed	4.2	0.77
H <sub>2</sub> O trap/HC trap/Catalyst, low CO feed	1.9	0.12
H <sub>2</sub> O trap/HC trap/catalyst, high CO feed	0.40	0.0

[0040] We believe that the results shown in Table 2 demonstrate the effectiveness of increasing the CO exotherm

by increasing the CO content in the system of the invention, and that this method, running generally counter to current emission control concepts, offers very substantial benefits. We believe that this is because the increased exotherm caused a rapid temperature rise of the catalyst to the catalyst light-off point. The system is therefore desirably optimised to provide that hydrocarbons are trapped until the catalyst has been heated by the CO exotherm, to the hydrocarbon light-off temperature.

[0041] One preferred embodiment of an emission control system according to the invention, is shown schematically in Figure 9. The exhaust gases from the engine are passed to an exhaust after-treatment system comprising a water trap, a hydrocarbon trap and a catalyst system. Desirably the catalyst is a CO low light-off catalyst. In order to obtain maximum benefits, the after-treatment system is dried before each start-up. This may be accomplished by utilising an air pump taking ambient air and passing it through a second molecular sieve water trap (eg zeolite 5A) which is heated by residual engine heat, and which continues to operate after engine switch-off. The secondary molecular sieve is itself dried during normal engine operation by the combination of residual engine heat and a flow of air, and after engine switch-off the secondary molecular sieve and pump provides hot dried air to dry the after-treatment system.

#### TEST 10

[0042] The benefits of the invention have been demonstrated in engine tests, using a US Ford Contour, model year 1994 and with a 2 litre engine, in which the exhaust system incorporates two 42in<sup>3</sup> (688cc) monoliths. The second (downstream) monolith had deposited thereon H-ZSM5 as a hydrocarbon absorber. In the initial tests, no water trap was deposited on the first monolith, but the bare monolith was retained in the system to keep the back-pressure and thermal mass constant. In the second series of tests, a zeolite 5A was deposited on the first monolith. The tests were run to assess the capability of the system to trap total hydrocarbons, and the car engine and exhaust system were operated in five FTP tests. No measurements were made during the first FTP tests, in order to "age" the system. After the first and second tests, the system was allowed to cool normally after engine switch-off, and the results for hydrocarbon trapped were measured for the second and third FTP tests, and averaged to give the results labelled "not pre-dried" in Table 3 below. After the third and fourth tests, nitrogen was flowed through the exhaust system to substantially eliminate moisture in the trapping system. This mimics the effect of using a water-trap to dry air used to dry the HC-trap and/or the catalyst. The results from the fourth and fifth FTP tests, therefore, have been averaged and the results for hydrocarbon trapping are labelled "pre-dried" in Table 3.

TABLE 3:

Hydrocarbon Trapping (%)		
water trap/HC trap/pre-dried?	0-20 seconds	20-40 seconds
blank/yes/not pre-dried	36.7	8.4
blank/yes/pre-dried	47.0	13.6
yes/yes/not-pre-dried	52.1	1.5
yes/yes/pre-dried	70.5	0.6

[0043] It is plain that pre-drying of the blank/HC trap system shows a clear advantage in HC trap performance, and trapping in both portions of the test were improved. In the case of the water trap/HC trap system, this shows an improvement in HC trapping efficiency even when not pre-dried, but pre-drying demonstrates a significant improvement. Further studies and theoretical calculations indicate that the 70.5% trapping in the first 20 seconds probably represent trapping of all HC's larger than C<sub>2</sub>.

[0044] The above Tests describe various aspects of the present invention, but these may be changed in detail without departing from the features defined in the claims.

#### Claims

1. An emission control system for an internal combustion engine, which system comprising an emission control catalyst and a trap for hydrocarbons (HC) the HC trap being either positioned upstream of the catalyst or co-located with the catalyst, and drying means comprising means for flowing a stream of air over the HC trap and/or the catalyst thereby to dry the HC trap and/or the catalyst and means in use, to operate the drying means after engine

switch-off or before cold-start, wherein the system further includes a water trap to dry the air used to dry the HC trap and/or the catalyst.

2. A system according to claim 1, wherein the supply means includes means for heating the air.
3. A system according to any preceding claim, wherein the HC trap also has NO<sub>x</sub>-trap activity.
4. A system according to any preceding claim, wherein the catalyst is a CO oxidation catalyst and, preferably is based on platinum or palladium.
5. A system according to claim 4, wherein the HC trap is co-located with the CO oxidation catalyst, wherein the HC trap is mixed with or layered over the CO oxidation catalyst, the arrangement being such that CO and O<sub>2</sub> is permitted to, but HC is prevented from, reaching the CO oxidation catalyst.
6. A system according to any preceding claim, wherein the HC trap includes an ion-exchanged zeolite, Co/ZSM-5, Pt/ZSM-5, an impregnated zeolite, a non-metalised zeolite, silicate or an aluminosilicate.
7. A system according to any preceding claim, further comprising a water trap disposed upstream of the HC trap.
8. A system according to any preceding claim, further comprising a water trap disposed downstream of the catalyst.
9. A system according to claim 7 or 8, wherein the water trap includes zeolite 5A, zeolite 3A, zeolite 4A or zeolite 13X.
10. A system according to any preceding claim, further comprising engine management means pre-programmed to run the engine during cold-start to provide an increased concentration of CO to the catalyst relative to normal running conditions.
11. A method of reducing polluting emissions from engine exhaust gas, which method comprising passing said exhaust gas through a system including, in order, a hydrocarbon (HC) trap and an emission control catalyst and drying said trap and/or catalyst after engine switch-off or before cold start by flowing a stream of dry air thereover, whereby the air is dried using a water trap.
12. A method according to claim 12, wherein after start-up, the exhaust gas is passed through a water trap before the HC trap.
13. A method according to claim 11 or 12, wherein drying is effected by flowing a stream of heated dried air through the HC trap and/or the catalyst after engine switch-off.
14. A method according to claim 11, 12 or 13, wherein the catalyst comprises a CO oxidation catalyst, preferably based on platinum or palladium, and the CO oxidation exotherm is used to raise the temperature of the catalyst sufficiently high to oxidise HCs as said HCs are desorbed from the HC trap.
15. A method according to claim 14, further comprising the step of preventing contact of the CO oxidation catalyst with HCs and/or NO whereby inhibition of CO oxidation inhibition thereby is prevented.

#### Patentansprüche

1. Emissionssteuerungssystem für einen Verbrennungsmotor, das einen Emissionssteuerungskatalysator und eine Falle für Kohlenwasserstoffe (HC), wobei die HC-Falle entweder stromauf des Katalysators angeordnet ist oder mit dem Katalysator gemeinsam angeordnet ist, und Trocknungsmittel, die Mittel, um einen Luftstrom über die HC-Falle und/oder den Katalysator strömen zu lassen, so dass die HC-Falle und/oder der Katalysator getrocknet wird, umfassen, und Mittel zur Verwendung, um die Trocknungsmittel nach Abschalten des Motors oder vor einem Kaltstart zu betätigen, umfasst, wobei das System des weiteren eine Wasserfalle umfasst, um die zum Trocknen der HC-Falle und/oder des Katalysators verwendete Luft zu trocknen.
2. System nach Anspruch 1, wobei die Zuspeismittel Mittel zum Erwärmen der Luft umfassen.

3. System nach einem der vorhergehenden Ansprüche, wobei die HC-Falle auch eine NO<sub>x</sub>-Fallen-Aktivität aufweist.
4. System nach einem der vorhergehenden Ansprüche, wobei der Katalysator ein CO-Oxidationskatalysator ist und vorzugsweise auf Platin oder Palladium basiert.
5. System nach Anspruch 4, wobei die HC-Falle zusammen mit dem CO-Oxidationskatalysator angeordnet ist, wobei die HC-Falle mit dem CO-Oxidationskatalysator vermischt ist oder als Schicht über dem CO-Oxidationskatalysator angeordnet ist, wobei die Anordnung so ist, dass es erlaubt ist, dass CO und O<sub>2</sub> den CO-Oxidationskatalysator erreicht, es jedoch verhindert wird, dass die Kohlenwasserstoffe (HC) den CO-Oxidationskatalysator erreichen.
6. System nach einem der vorhergehenden Ansprüche, wobei die HC-Falle einen ionenausgetauschten Zeolith, Co/ZSM-5, Pt/ZSM-5, einen imprägnierten Zeolith, einen nicht-metallisierten Zeolith, Sillcat oder ein Aluminosilicat umfasst.
7. System nach einem der vorhergehenden Ansprüche, das des weiteren eine stromauf der HC-Falle angeordnete Wasserfalle umfasst.
8. System nach einem der vorhergehenden Ansprüche, das des weiteren eine stromab des Katalysators angeordnete Wasserfalle umfasst.
9. System nach Anspruch 7 oder 8, wobei die Wasserfalle Zeolith 5A, Zeolith 3A, Zeolith 4A oder Zeolith 13X umfasst.
10. System nach einem der vorhergehenden Ansprüche, das des weiteren Motormanagementmittel umfasst, die so vorprogrammiert sind, dass der Motor während des Kaltstarts so gefahren wird, dass dem Katalysator, bezogen auf die normalen Laufbedingungen, eine erhöhte CO-Konzentration bereitgestellt wird.
11. Verfahren zur Verringerung von Schadstoffemissionen aus dem Motorabgas durch Führen des Abgases durch ein System, das in der angegebenen Reihenfolge eine Kohlenwasserstoff (HC)-Falle und einen Emissionssteuerungskatalysator umfasst, und Trocknen der Falle und/oder des Katalysators nach Abschalten des Motors oder vor einem Kaltstart, indem ein Strom von trockener Luft darüber geführt wird, wodurch die Luft unter Verwendung einer Wasserfalle getrocknet wird.
12. Verfahren nach Anspruch 11, wobei nach dem Start das Abgas durch eine Wasserfalle vor der HC-Falle geführt wird.
13. Verfahren nach Anspruch 11 oder 12, wobei das Trocknen erfolgt, indem ein Strom von erwärmter getrockneter Luft durch die HC-Falle und/oder den Katalysator nach Abschalten des Motors geführt wird.
14. Verfahren nach Anspruch 11, 12 oder 13, wobei der Katalysator einen CO-Oxidationskatalysator umfasst und vorzugsweise auf Platin oder Palladium basiert und die CO-Oxidationsexothermie verwendet wird, um die Temperatur des Katalysators ausreichend hoch anzuheben, um die Kohlenwasserstoffe (HCs) zu oxidieren, wenn die HCs von der HC-Falle desorbiert werden.
15. Verfahren nach Anspruch 14, das ferner die Stufe umfasst, dass der Kontakt des CO-Oxidationskatalysators mit den Kohlenwasserstoffen (HCs) und/oder NO verhindert wird, wodurch die Hemmung der CO-Oxidation erreicht wird.

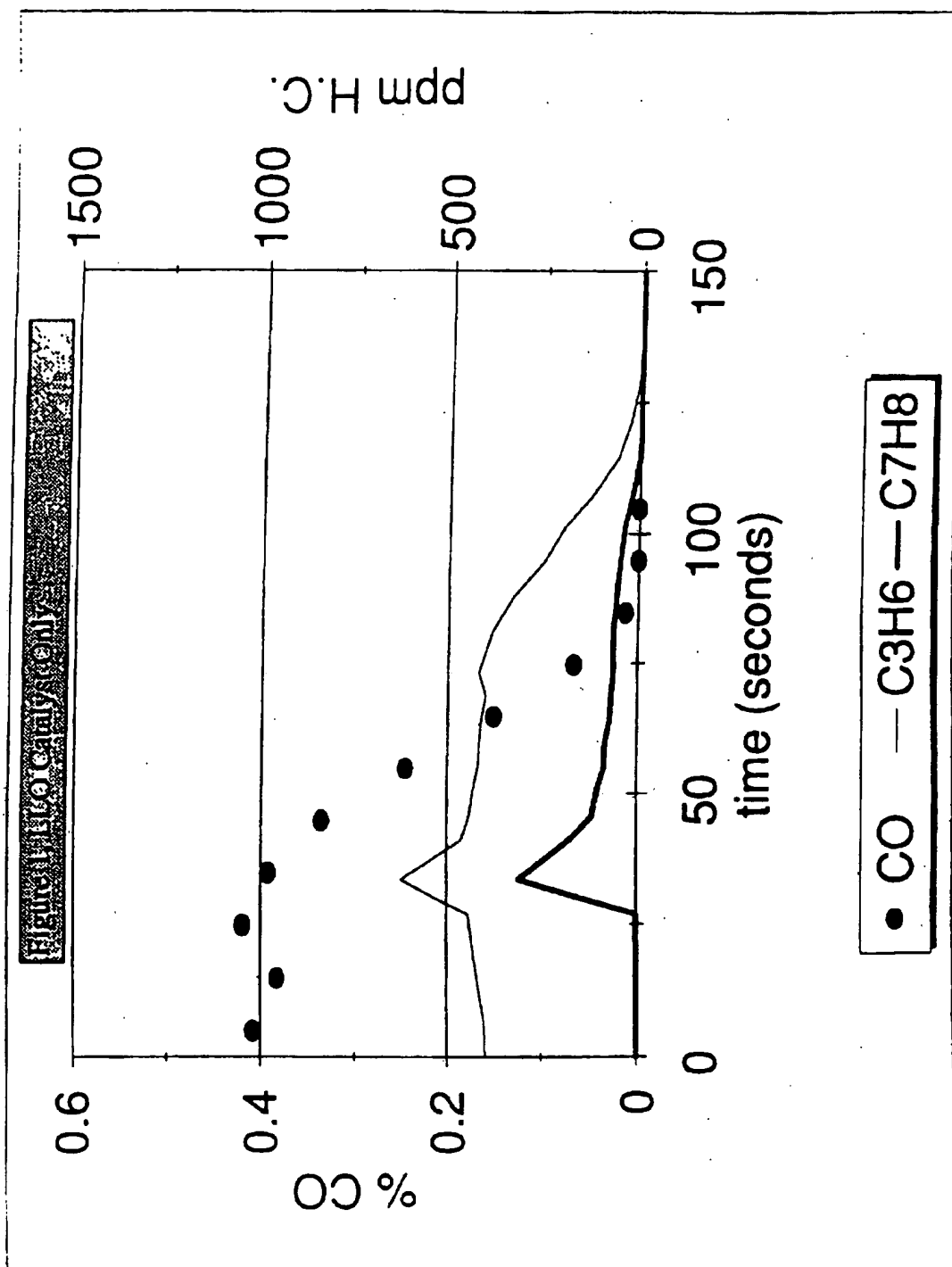
#### Revendications

1. Système de commande d'émissions pour un moteur à combustion interne, lequel système comporte un catalyseur de commande d'émissions et un piège pour hydrocarbures (HC), le piège HC étant positionné en amont du catalyseur ou au même niveau que le catalyseur, et des moyens de séchage comportant des moyens pour faire écouler un courant d'air sur le piège HC et/ou le catalyseur de manière à sécher le piège HC et/ou le catalyseur et des moyens en utilisation pour actionner les moyens de séchage après un arrêt du moteur avant un démarrage à froid, dans lequel le système comporte de plus un sécheur de vapeur pour sécher l'air utilisé pour sécher le piège HC et/ou le catalyseur.

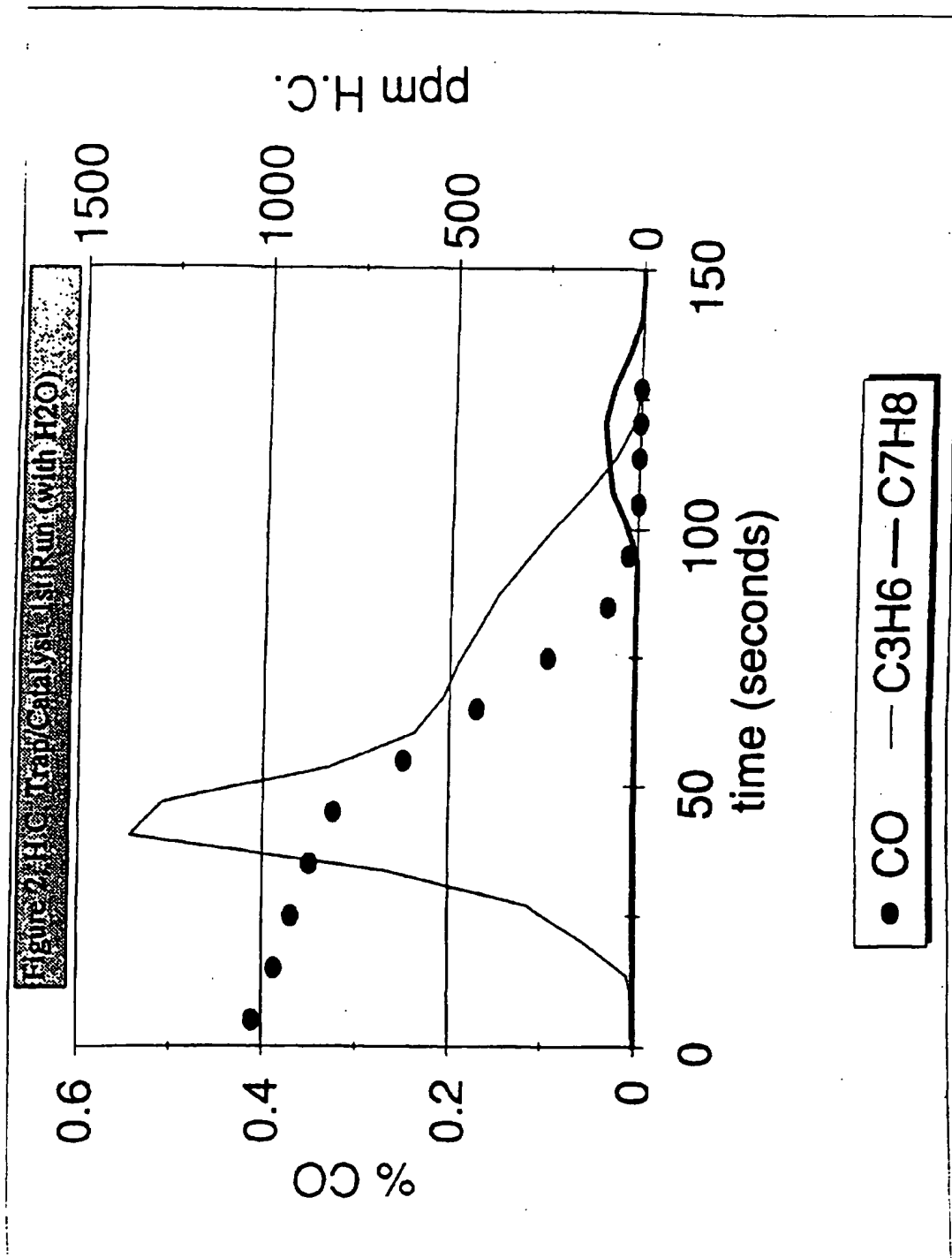


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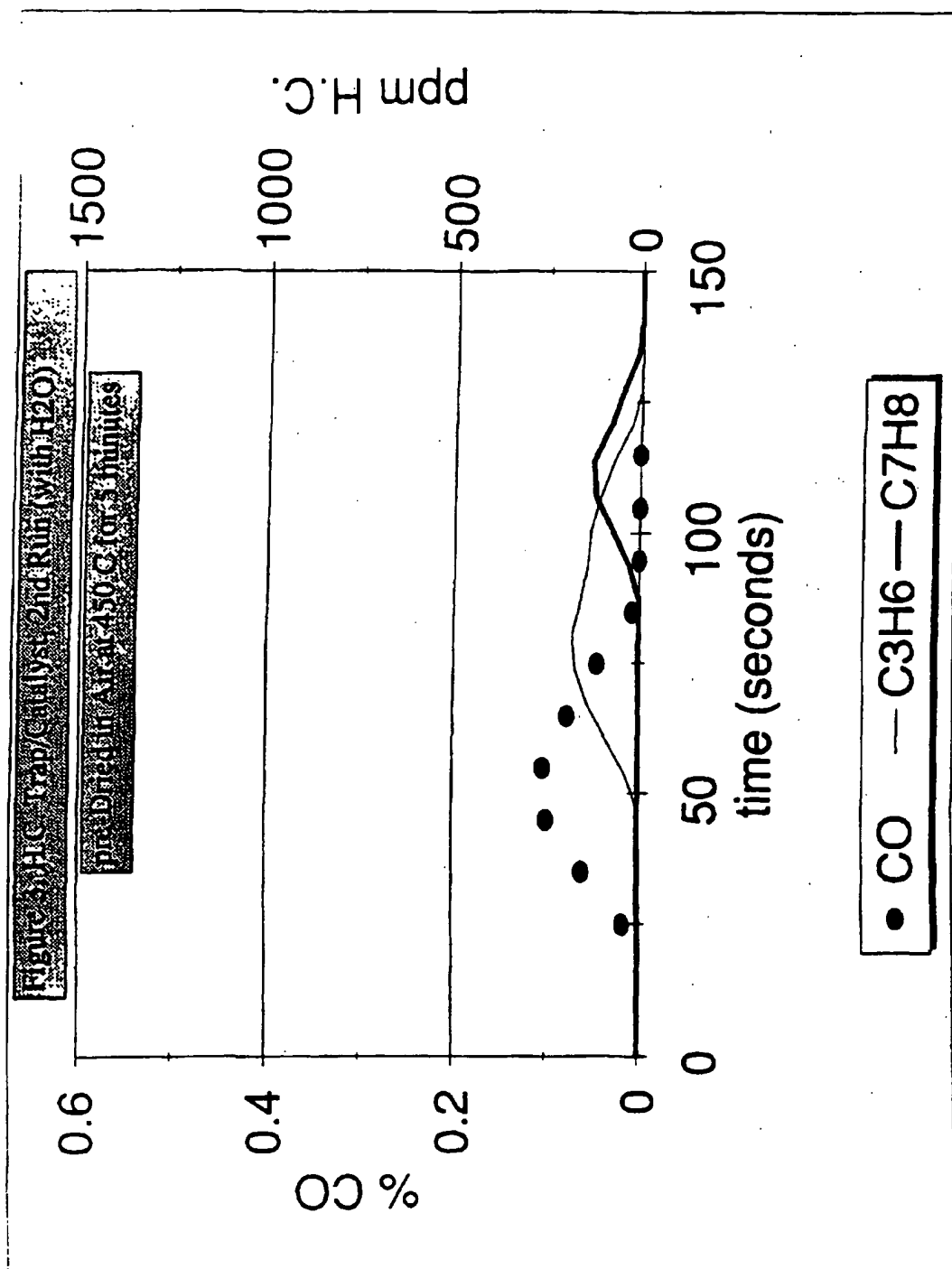
2. Système selon la revendication 1, dans lequel les moyens d'alimentation comportent des moyens pour chauffer l'air.
3. Système selon l'une quelconque des revendications précédentes, dans lequel le piège HC a également une activité de piégeage des NOx.
4. Système selon l'une quelconque des revendications précédentes, dans lequel le catalyseur est un catalyseur d'oxydation de CO et, de préférence, est basé sur du platine ou du palladium.
5. Système selon la revendication 4, dans lequel le piège HC est situé au même niveau que le catalyseur d'oxydation de CO, dans lequel le piège HC est mélangé avec le catalyseur d'oxydation de CO, ou stratifié sur celui-ci, l'agencement étant tel que CO et O<sub>2</sub> sont autorisés à atteindre le catalyseur d'oxydation de CO, mais les HC ne peuvent pas atteindre celui-ci.
6. Système selon l'une quelconque des revendications précédentes, dans lequel le piège HC comporte une zéolite à ions échangés, Co/ZSM-5, Pt/ZSM-5, une zéolite imprégnée, une zéolite non-métallisée, une silice ou une alu-mino-silice.
7. Système selon l'une quelconque des revendications précédentes, comportant de plus un sécheur de vapeur disposé en amont du piège HC.
8. Système selon l'une quelconque des revendications précédentes, comportant de plus un sécheur de vapeur disposé en aval du catalyseur.
9. Système selon la revendication 7 ou 8, dans lequel le sécheur de vapeur inclut une zéolite 5A, une zéolite 3A, une zéolite 4A ou une zéolite 13X.
10. Système selon l'une quelconque des revendications précédentes, comportant de plus des moyens de gestion de moteur préprogrammés pour activer le moteur pendant un démarrage à froid afin de fournir une concentration accrue de CO dans le catalyseur par rapport à des conditions de fonctionnement normales.
11. Procédé pour réduire des émissions polluantes depuis un gaz d'échappement de moteur, lequel procédé comporte le passage dudit gaz d'échappement à travers un système incluant, dans cet ordre, un piège à hydrocarbures (HC), et un catalyseur de commande d'émissions et le séchage dudit piège et/ou du catalyseur après arrêt du moteur, ou avant un démarrage à froid pour faire s'écouler un courant d'air sec dessus, de sorte que l'air est séché en utilisant un sécheur de vapeur.
12. Procédé selon la revendication 12, dans lequel, après démarrage, le gaz d'échappement est passé à travers un sécheur de vapeur avant le piège HC.
13. Procédé selon la revendication 11 ou 12, dans lequel le séchage est effectué en faisant s'écouler un courant d'air séché chauffé à travers le piège HC et/ou le catalyseur après arrêt du moteur.
14. Procédé selon la revendication 11, 12 ou 13, dans lequel le catalyseur comporte un catalyseur d'oxydation de CO, de préférence basé sur du platine ou du palladium, et l'exothermicité d'oxydation de CO est utilisée pour augmenter la température du catalyseur à un niveau suffisamment élevé pour oxyder les HC lorsque lesdits HC sont désorbés depuis le piège HC.
15. Procédé selon la revendication 14, comportant de plus l'étape consistant à empêcher le contact du catalyseur d'oxydation de CO avec les HC et/ou NO de sorte que l'inhibition d'une inhibition d'oxydation de CO est ainsi évitée.

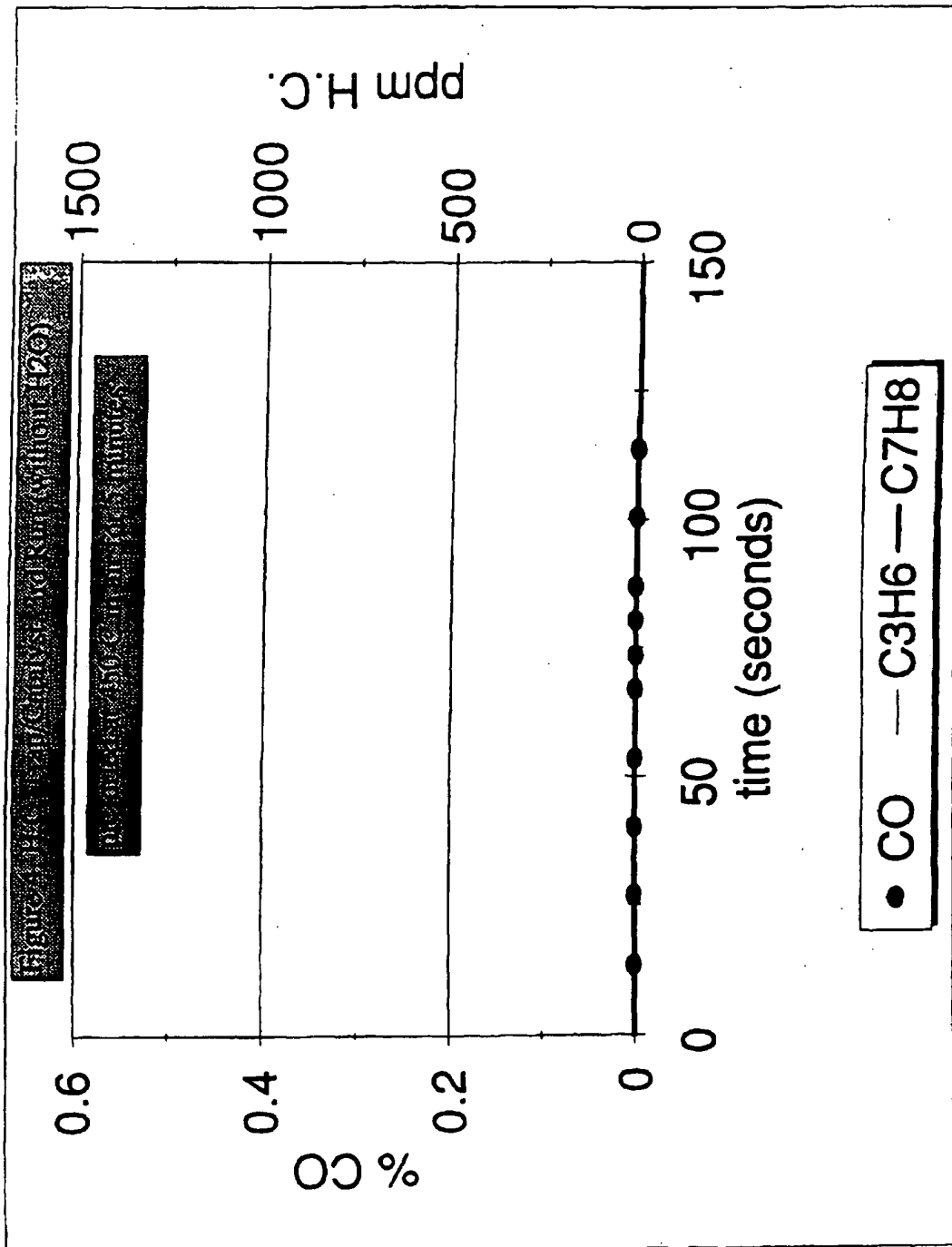


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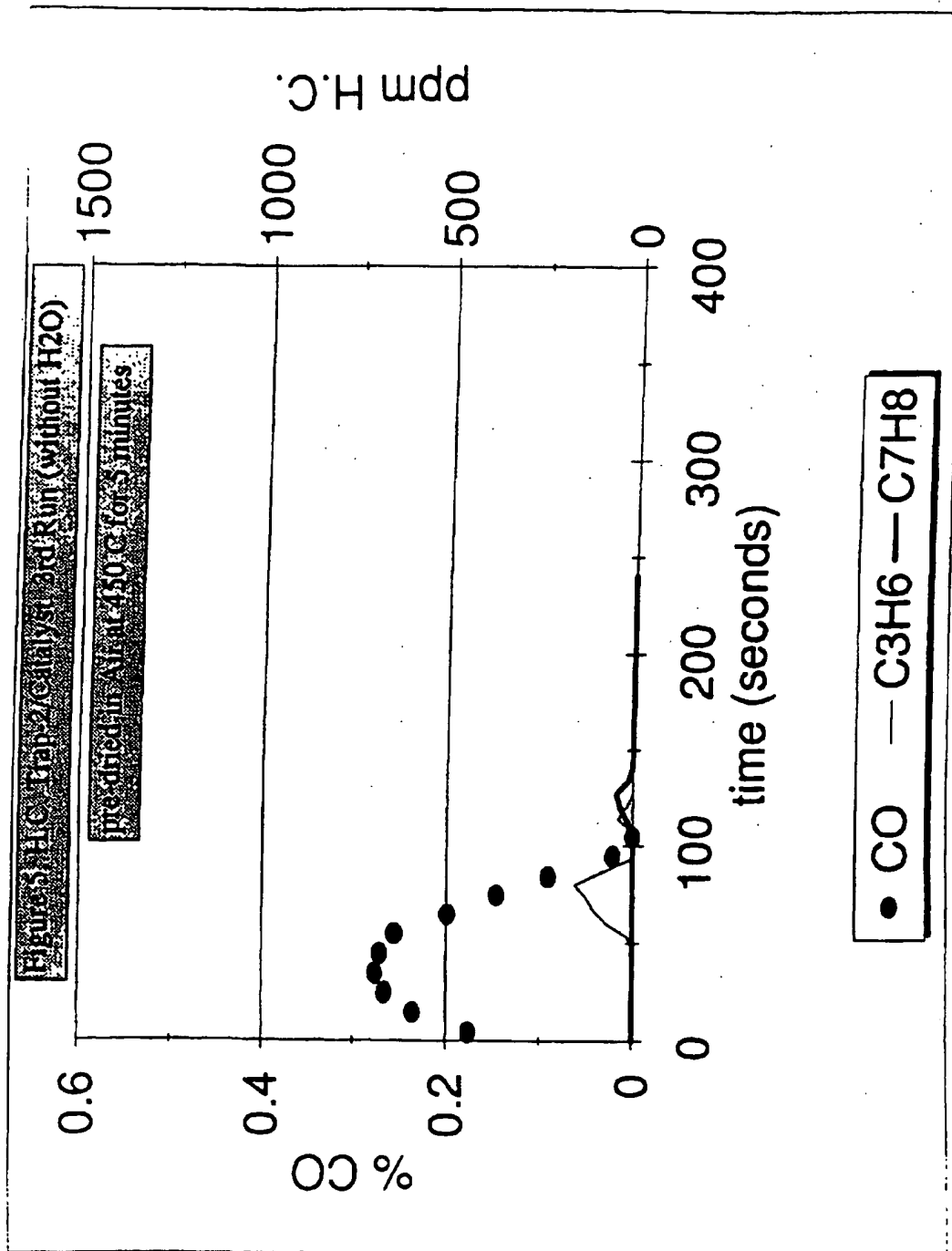


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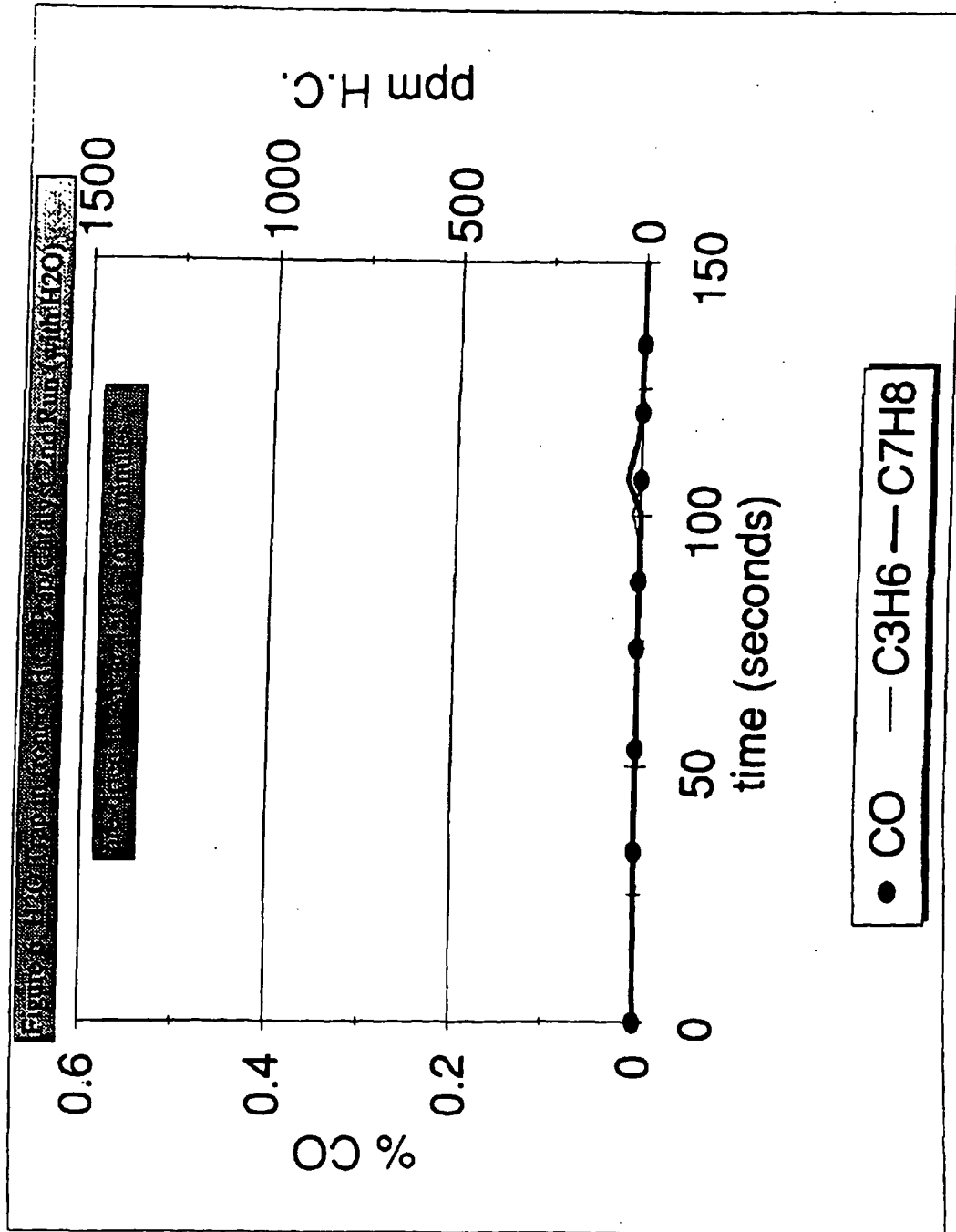




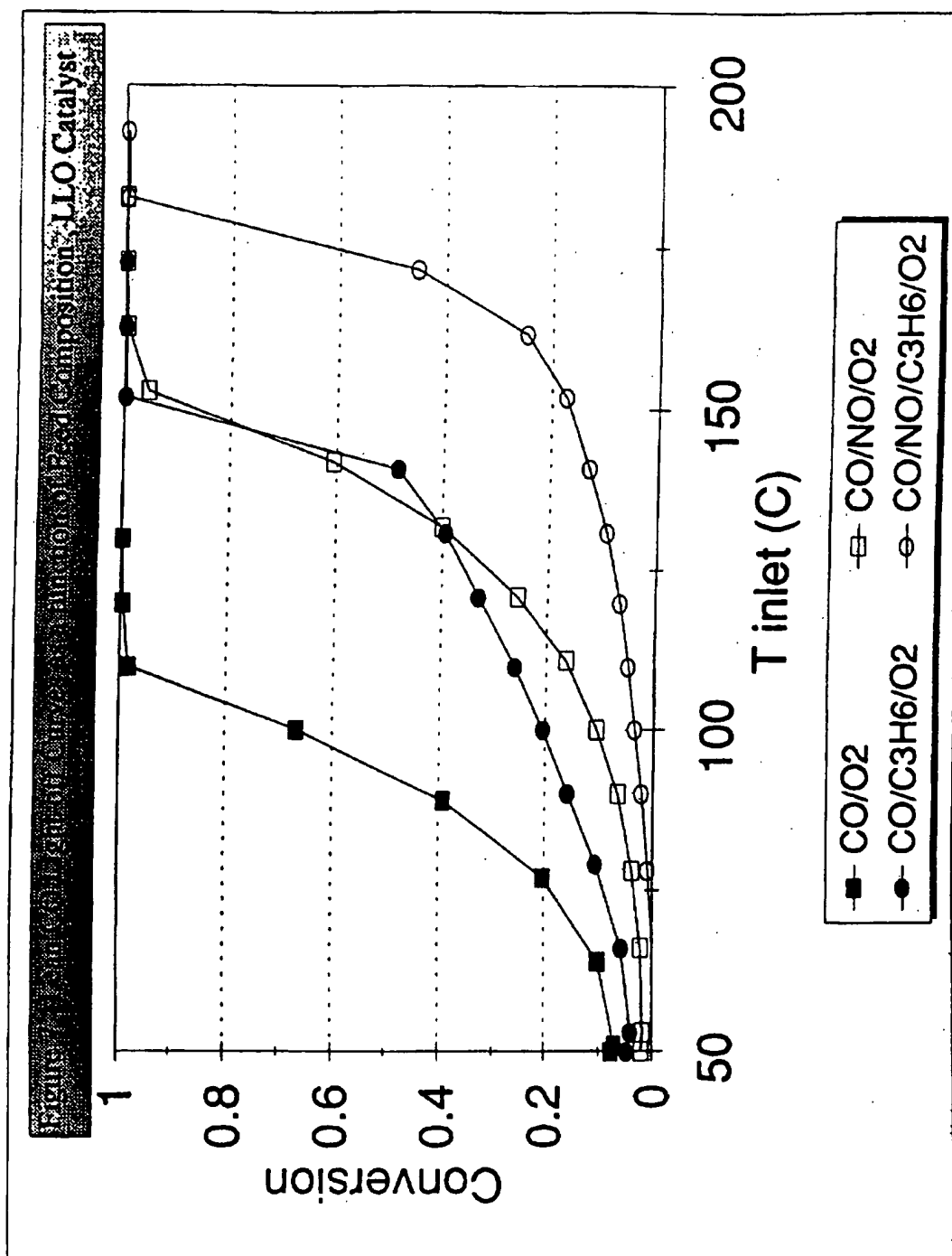
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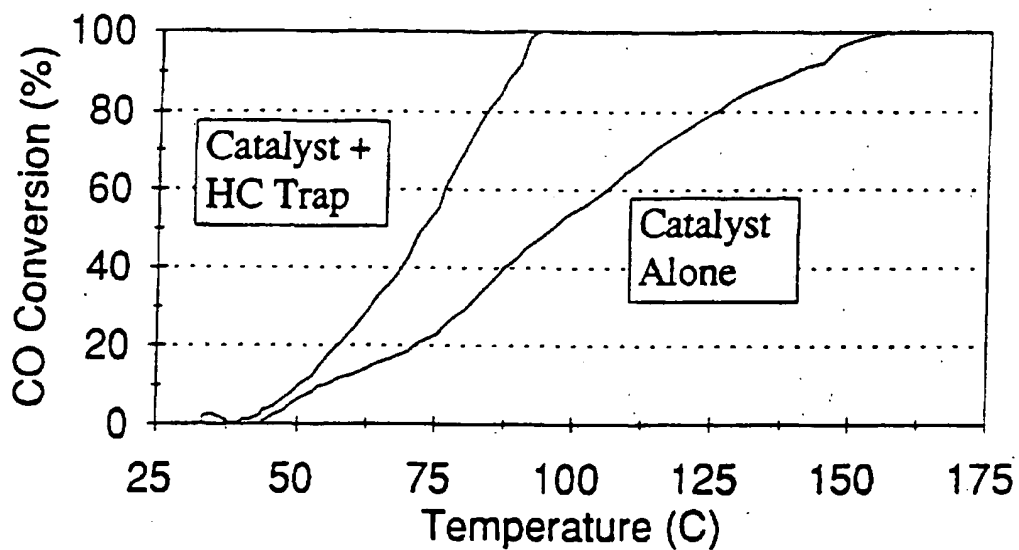
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### Use of a HC Trap to Remove the HC Inhibition of the CO Oxidation Reaction



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**Figure 9**  
**Exhaust Aftertreatment System**

